

# Protein Adsorption

This application simulates an ion-exchange column for protein adsorption. The fluid phase contains four components: two proteins, solvent, and one salt. The adsorption/desorption kinetics is described by two equilibrium reactions where proteins displace ions adsorbed at the surface and vice versa.

The example highlights how reactions at chemical equilibrium can be studied in a 0D reactor system in Reaction Engineering. In addition, it also shows how the kinetics from the 0D setup is exported to a 3D model where the reacting surface in the column can be studied in detail. The 3D model incorporates mass transport through diffusion and convection, and the reactions at the surface of the ion-exchange mass with Transport of Diluted Species, Laminar Flow, and Surface Reactions interfaces.

# Introduction Protein Ion-Exchange

The binding of proteins to ion exchangers can be described within the steric mass action approximation (SMA). This approach assumes that the adsorption of a protein can be considered as an exchange reaction of the protein with a given number of adsorbed ions.

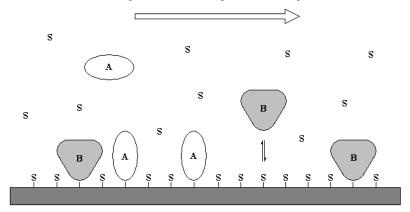


Figure 1: Proteins A and B displacing salt ions S at an ion-exchanger surface.

The equilibrium describing the adsorption/desorption reactions is

$$S(ads) + P \Leftrightarrow P(ads) + S \tag{1}$$

Here, S denotes the salt ion, P stands for either protein A and B. Once P is adsorbed, P(ads), salt ions are displaced, reducing the concentration of adsorbed salt ions, S(ads).

# Model Definition

The system is modeled both in 0D and in 3D. The former model setup is adequate to investigate the kinetics of the equilibrium reactions within the column. The latter makes it possible to study the surface of the ion-exchange beads that make up the porous structure of the ion-exchange mass. In Figure 2, the two model approaches are presented.

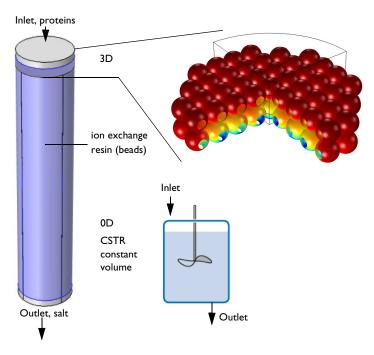


Figure 2: Ion-exchange column and model geometries. The 0D model approximates the entire column, while the 3D geometry is a detailed representation of a section at the top of the column.

The 0D model utilizes the reactor type CSTR, constant volume in the Reaction Engineering interface. Ideal conditions are assumed within the reactor, meaning that wellmixed conditions with no concentration gradients apply. The reaction kinetics are described by Equation 1 for proteins A and B are entered directly into the interface as equilibrium surface reactions. The equilibrium constants for reaction 1, adsorption of A, is  $K_1^{eq} = 2$  and for reaction 2, adsorption of B, is  $K_2^{eq} = 5$ . These are entered as well, relating the concentrations as followed

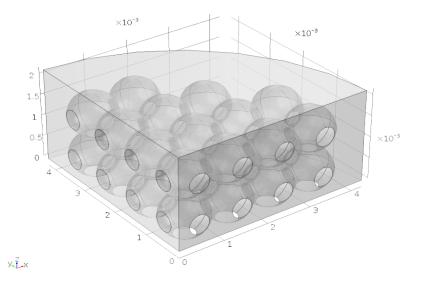
$$K_1^{\rm eq} = \frac{c_S c_{A(\rm ads)}}{c_A c_{S(\rm ads)}} \tag{2}$$

$$K_2^{\rm cq} = \frac{c_S c_{B(\rm ads)}}{c_B c_{S(\rm ads)}} \tag{3}$$

In order to compute the concentrations, both protein surface concentrations need to be set as dependent in the Equilibrium Species Vector section.

The proteins enter the reactor with a Feed Inlet with concentrations that vary in accordance to a 10 s Gaussian pulse with a maximum of 0.05 mol/m<sup>3</sup>. The outlet flow rate regulates so that the volume of the reactor is constant. Initially, no protein is available in the column and the ion-exchange mass is set to be completely adsorbed with salt, i.e. the initial site density,  $\gamma_0$ , is equal to the initial surface concentration of S, S(ads).

For the 3D model, as shown in Figure 3, only one quarter of the top section of the column is simulated due to symmetry. The proteins enter the top with a constant concentration of  $0.05 \text{ mol/m}^3$ . In the column initially, the pores (the bulk) is filled with solvent and the ion-exchange beads are saturated with adsorbed salt.



# Figure 3: 3D model geometry.

The reaction kinetics are taken directly from the 0D model with the Generate Space-Dependent Model feature and are collected in a Chemistry interface that also supplies computed diffusion coefficients and fluid density for the 3D setup. The mass balances describing the species mass transport in the pores of the column are set up with the Transport of Diluted Species interface with diffusion and convection accounted for

$$\frac{\partial c_i}{\partial t} + \nabla \cdot (-D_i \nabla c_i) + \mathbf{u} \cdot \nabla c_i = 0$$
(4)

On the right hand side of Equation 4 no reaction source is present for the bulk. However, the surface of the ion-exchange beads produces a reaction source that needs to be coupled to this equation. This is simply done with a Surface Reaction interface. Such an interface is automatically generated with the use of the Generate Space-Dependent Model feature if surface reactions are present.

The 3D model also computes the convective velocity, u, with a Laminar Flow interface. The velocity is based on the assumption that the velocity, U, within the reactor is 0.1 mm/ s and that the inlet is open to the surroundings, i.e. exposed to the atmospheric pressure.

# STUDY SETTINGS

The 3D problem is solved in a two-step study. First, the Laminar Flow interface is first solved with a Stationary study step. Second, the rest of the interfaces (Chemistry, Transport of Diluted Species, and Surface Reactions) are solved with a Time Dependent study step. A Fully Coupled Direct solver is required in the second step to obtain stable computations.

# Study 1 — Space Independent

Figure 4 shows how the concentrations of the reacting species change with the time. Initially, only adsorbed salt species are present in the column. The concentrations of proteins A and B are seen to change with the Gaussian concentration pulse feed inlet. A stronger adsorption affinity of protein B compared to protein A is readily observed. Note also how the concentration of bulk salt species S increases as the proteins adsorb at the surface. Toward the end of the pulse, most proteins have been adsorbed in the column and the bulk salt species have exited the system.

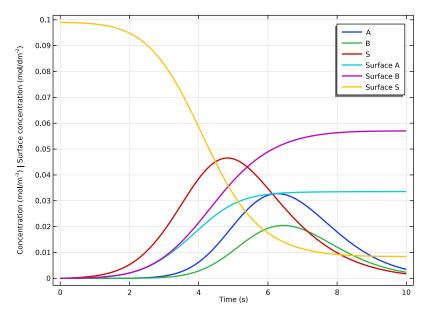


Figure 4: Concentrations of the reacting species as functions of time (s).

# Study 2 — Space Dependent

The 3D model is solved for 30 s and a selection of the results are displayed in this section. Figure 5, Figure 6, Figure 7, and Figure 8 show the behavior of protein B after 5 s and 30 s.

From Figure 6, in which the bulk concentration is shown, indicates that the beads at the center of the column are less accessible for adsorption or that the protein is more rapidly adsorbed at the center, both phenomena lowering the bulk concentration there.

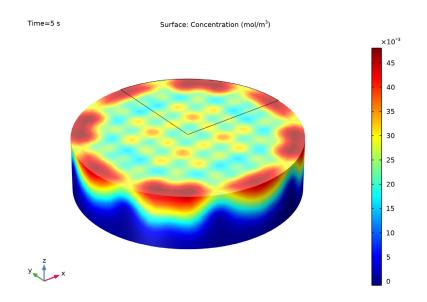


Figure 5: Bulk concentration of B at 5 s.

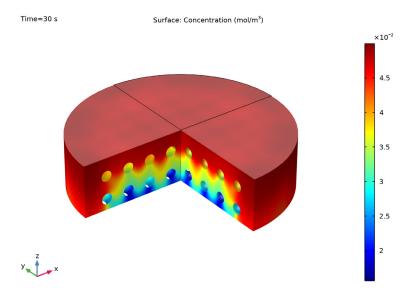


Figure 6: Bulk concentration of B at 30 s.

To get a proper understanding of the ion-exchange beads, a comparison of the adsorbed B surface concentration at the two times is also made with the results in Figure 7 and Figure 8. The lower surface concentration of B in the center suggests that less B is adsorbed there and that the porous structure obstructs the species transport. Note that the bead surface cannot adsorb more than the (initial) site density of the ion-exchange material,  $\gamma_0$  (SI unit: mol/m<sup>2</sup>).

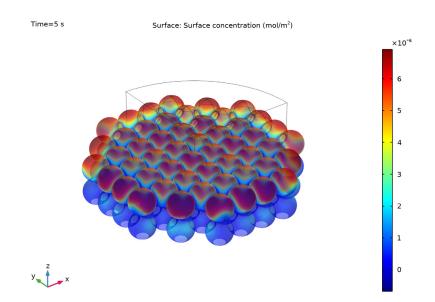


Figure 7: Surface concentration of B at 5 s.

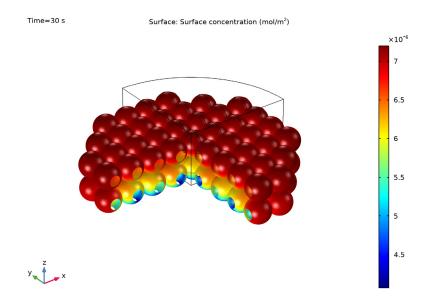


Figure 8: Surface concentration of B at 30 s.

In Figure 9, the velocity field is displayed. It shows that the porous structure causes a quite distorted velocity field. The exception is at the walls where the flow is less obstructed due to the relatively large gap between beads and wall.

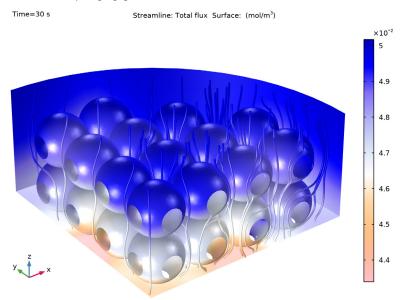


Figure 9: Velocity field in the pores of the column section.

**Application Library path:** Chemical\_Reaction\_Engineering\_Module/ Mixing\_and\_Separation/protein\_adsorption

# Modeling Instructions

From the File menu, choose New.

### NEW

In the New window, click 🖉 Model Wizard.

# MODEL WIZARD

I In the Model Wizard window, click • 0D.

2 In the Select Physics tree, select Chemical Species Transport>Reaction Engineering (re).

- 3 Click Add.
- 4 Click 🔿 Study.
- 5 In the Select Study tree, select General Studies>Time Dependent.
- 6 Click 🗹 Done.

# GLOBAL DEFINITIONS

Import the model parameters from a file from the application's Application Library folder.

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- 3 Click 📂 Load from File.
- 4 Browse to the model's Application Libraries folder and double-click the file protein\_adsorption\_parameters.txt.

## Gaussian Pulse I (gpl)

Reactants are injected to the system in a pulse. Choose a **Gaussian Pulse** function to describe the injection.

- I In the Home toolbar, click f(x) Functions and choose Global>Gaussian Pulse.
- 2 In the Settings window for Gaussian Pulse, locate the Parameters section.
- **3** In the **Location** text field, type **5**.
- 4 In the Standard deviation text field, type 1.5.

Use the **Gaussian Pulse** function to set up a time-dependent pulse variable with an amplitude of 1.

# DEFINITIONS

Variables I

- I In the Model Builder window, under Component I (compl) right-click Definitions and choose Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- **3** In the table, enter the following settings:

Name	Expression	Unit	Description
pulse11	3.76*gp1(t/1[s])		Pulse with amplitude 1

#### REACTION ENGINEERING (RE)

Select a constant volume CSTR to model the ion-exchange column in 0D.

- I In the Model Builder window, under Component I (compl) click Reaction Engineering (re).
- 2 In the Settings window for Reaction Engineering, locate the Reactor section.
- 3 From the Reactor type list, choose CSTR, constant volume.
- 4 Locate the Mixture Properties section. From the Phase list, choose Liquid.

#### Reaction 1

Set up the equilibrium reaction for adsorption/desorption of protein A.

- 2 In the Settings window for Reaction, locate the Reaction Formula section.
- 3 In the Formula text field, type S(ads)+A=S+A(ads).
- 4 Click Apply.
- **5** Locate the **Equilibrium Settings** section. In the  $K_{eq0}$  text field, type Keq01.

Reaction 2

I In the Reaction Engineering toolbar, click 👗 Reaction.

In similar fashion, set up the equilibrium reaction for adsorption/desorption of protein B.

- 2 In the Settings window for Reaction, locate the Reaction Formula section.
- **3** In the **Formula** text field, type S(ads)+B=S+B(ads).
- 4 Click Apply.
- **5** Locate the **Equilibrium Settings** section. In the  $K_{eo0}$  text field, type Keq02.

Replace the default dependent variables and replace these with **A(ads)** and **B(ads)**. This omits any cyclic dependence of the reaction rates.

- 6 In the Model Builder window, click Reaction Engineering (re).
- 7 In the Settings window for Reaction Engineering, click to expand the Equilibrium Species Vector section.
- 8 In the Predefined dependent species (separated by ':') text field, type A(ads):B(ads).
- **9** Locate the **Reactor** section. Find the **Mass balance** subsection. From the **Volumetric rate** list, choose **User defined**.

Set vp=0, to neglect the volumetric production rate.

**IO** In the  $v_{\rm p}$  text field, type 0.

Select the reactive surface area available in the reactor. This regulates, when multiplied with the site density, how much the ion-exchange column can adsorb.

II Find the Surface reaction area subsection. In the  $A_r$  text field, type Arsurf.

Initial Values 1

In the **Initial Values** feature, set all species except adsorbed S (**S(ads)**) to zero. Also, set the initial density of surface sites for the ion-exchange mass. Note that the latter property sets the upper limit of how many moles can be adsorbed. Assume that each species takes up one reactive site.

I In the Model Builder window, click Initial Values I.

- **2** In the **Settings** window for **Initial Values**, click to expand the **Surface Species Initial Values** section.
- **3** In the  $\Gamma_{\rm s}$  text field, type G0.
- **4** In the table, enter the following settings:

Species	Surface concentration (mol/m <sup>2</sup> )	Site occupancy number (I)
S(ads)	CSOsurf	1

Feed Inlet I

Last, in the OD model, add the **Feed Inlet** feature containing bulk species A and B. Add the concentration with the Gaussian pulse in the feed stream.

- I In the Reaction Engineering toolbar, click 🚽 Feed Inlet.
- 2 In the Settings window for Feed Inlet, locate the Feed Inlet Properties section.
- **3** In the  $v_{\rm f}$  text field, type vfp.
- **4** Locate the **Feed Inlet Concentration** section. In the **Feed inlet concentration** table, enter the following settings:

Species	Concentration (mol/m^3)	
Α	CAmax_inlet*pulse11	
В	CBmax_inlet*pulse11	

Enter densities and molar masses in the bulk species nodes.

Species: A

- I In the Model Builder window, click Species: A.
- 2 In the Settings window for Species, locate the General Parameters section.

- **3** In the M text field, type MA.
- **4** In the  $\rho$  text field, type rho\_p.

#### Species: S

- I In the Model Builder window, click Species: S.
- 2 In the Settings window for Species, locate the General Parameters section.
- **3** In the *M* text field, type MS.
- **4** In the  $\rho$  text field, type rho\_S.

#### Species: B

- I In the Model Builder window, click Species: B.
- 2 In the Settings window for Species, locate the General Parameters section.
- **3** In the M text field, type MB.
- **4** In the  $\rho$  text field, type rho\_p.

Enter also molar mass in the surface species nodes.

Surface species: S(ads)

- I In the Model Builder window, click Surface species: S(ads).
- 2 In the Settings window for Species, locate the General Parameters section.
- **3** In the *M* text field, type MS.

Surface species: A(ads)

- I In the Model Builder window, click Surface species: A(ads).
- 2 In the Settings window for Species, locate the General Parameters section.
- **3** In the M text field, type MA.

Surface species: B(ads)

- I In the Model Builder window, click Surface species: B(ads).
- 2 In the Settings window for Species, locate the General Parameters section.
- **3** In the M text field, type MB.

Solve the 0D model for 10 s.

### STUDY I

Step 1: Time Dependent

- I In the Model Builder window, under Study I click Step I: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.

- 3 In the **Output times** text field, type range(0,0.1,10).
- **4** In the **Home** toolbar, click **= Compute**.

# RESULTS

# Concentrations 0D model

Create Figure 4 in which all species concentrations are displayed.

- I In the **Settings** window for **ID Plot Group**, type Concentrations OD model in the **Label** text field.
- 2 Click to expand the Title section. From the Title type list, choose None.
- 3 Locate the Plot Settings section. Select the x-axis label check box.
- 4 Select the y-axis label check box.
- 5 In the associated text field, type Concentration (mol/m<sup>-3</sup>) | Surface concentration (mol/dm<sup>-2</sup>).

## Global I

- I In the Model Builder window, expand the Concentrations 0D model node, then click Global I.
- In the Settings window for Global, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>
   Reaction Engineering>re.c\_A Concentration mol/m<sup>3</sup>.
- 3 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering>re.c\_B Concentration mol/m<sup>3</sup>.
- 4 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (comp1)>Reaction Engineering>re.c\_S Concentration mol/ m<sup>3</sup>.
- 5 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering>re.csurf\_A\_surf Surface concentration mol/m<sup>2</sup>.
- 6 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering>re.csurf\_B\_surf Surface concentration mol/m<sup>2</sup>.
- 7 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering>re.csurf\_S\_surf Surface concentration mol/m<sup>2</sup>.

8 Locate the y-Axis Data section. In the table, enter the following settings:

Expression	Unit	Description
re.csurf_A_surf*1e4	mol/m^2	Surface concentration per square dm
re.csurf_B_surf*1e4	mol/m^2	Surface concentration per square dm
re.csurf_S_surf*1e4	mol/m^2	Surface concentration per square dm

9 Click to expand the Coloring and Style section. In the Width text field, type 2.

10 Click to expand the Legends section. From the Legends list, choose Manual.

**II** In the table, enter the following settings:

Legends
A
В
S
Surface A
Surface B
Surface S

# **12** In the **Concentrations 0D model** toolbar, click **O Plot**.

Continue setting up a space-dependent model to investigate the top section of the ionexchange column. Start by adding a solvent to the system. The solvent in these types of systems is often water.

# **REACTION ENGINEERING (RE)**

Species 1

- I In the Reaction Engineering toolbar, click 📩 Species.
- 2 In the Settings window for Species, locate the Species Name section.
- **3** In the text field, type H20.
- **4** Locate the **Species Type** section. From the list, choose **Solvent**.
- **5** Locate the **General Parameters** section. In the *M* text field, type MH20.
- **6** In the  $\rho$  text field, type rho\_H20.

# Initial Values 1

I In the Model Builder window, click Initial Values I.

- **2** In the Settings window for Initial Values, locate the Volumetric Species Initial Values section.
- **3** In the table, enter the following settings:

Species	Concentration (mol/m^3)
H2O	CH20

For a liquid system with solvent, several transport parameters can be computed within the **Chemistry** interface. Activate this functionality by following these steps.

- 4 In the Model Builder window, click Reaction Engineering (re).
- **5** In the **Settings** window for **Reaction Engineering**, click to expand the **Calculate Transport Properties** section.
- 6 Select the Calculate mixture properties check box.
- 7 From the Dynamic viscosity list, choose User defined.
- **8** In the  $\mu$  text field, type myH20.

Use the **Generate Space-dependent Model** feature to set up the space-dependent model. Select a 3D geometry and **Transport of Diluted Species** and **Laminar Flow** interfaces together with a **Time Dependent** study type.

#### Generate Space-Dependent Model I

- I In the Reaction Engineering toolbar, click 📫 Generate Space-Dependent Model.
- **2** In the **Settings** window for **Generate Space-Dependent Model**, locate the **Study Type** section.
- 3 From the Study type list, choose Time dependent.
- **4** Locate the **Physics Interfaces** section. Find the **Fluid flow** subsection. From the list, choose **Laminar Flow**: **New**.
- 5 Locate the Space-Dependent Model Generation section. Click Create/Refresh.

# GEOMETRY I(3D)

Insert the 3D geometry sequence file protein\_adsorption\_geom\_sequence.mph from the application's **Application Library** folder.

- I In the Model Builder window, expand the Component 2 (comp2) node, then click Geometry 1(3D).
- 2 In the Geometry toolbar, click **Insert Sequence**.
- **3** Browse to the model's Application Libraries folder and double-click the file protein\_adsorption\_geom\_sequence.mph.

4 In the Geometry toolbar, click 🟢 Build All.

**5** Click the  $4 \rightarrow$  **Zoom Extents** button in the **Graphics** toolbar.

#### TRANSPORT OF DILUTED SPECIES (TDS)

Start with the Transport of Diluted Species interface.

#### Transport Properties 1

The Laminar Flow interface is Coupled to the velocity field.

A and B enter the column at the top. Select **Danckwerts (Flux)** for a more stable computation.

Inflow I

- In the Model Builder window, expand the Component 2 (comp2)> Transport of Diluted Species (tds) node, then click Inflow 1.
- 2 In the Settings window for Inflow, locate the Boundary Selection section.
- 3 From the Selection list, choose Inlet.
- **4** Locate the **Concentration** section. In the  $c_{0,cA}$  text field, type CAmax\_inlet.
- **5** In the  $c_{0,cB}$  text field, type CBmax\_inlet.
- 6 Locate the Boundary Condition Type section. From the list, choose Flux (Danckwerts).

#### Outflow I

Set an **Outflow** condition at the bottom of the geometry. This means that the transport along the z direction (the height) of the reactor is dominated by convection.

- I In the Model Builder window, click Outflow I.
- 2 In the Settings window for Outflow, locate the Boundary Selection section.
- **3** From the Selection list, choose Outlet column section.

#### Surface Equilibrium Reaction 1

The surface of the beads is the boundary where reactions take place.

- I In the Model Builder window, click Surface Equilibrium Reaction I.
- **2** In the **Settings** window for **Surface Equilibrium Reaction**, locate the **Boundary Selection** section.
- **3** From the **Selection** list, choose **Array I**.

#### Surface Equilibrium Reaction 2

I In the Model Builder window, click Surface Equilibrium Reaction 2.

- **2** In the Settings window for Surface Equilibrium Reaction, locate the Boundary Selection section.
- 3 From the Selection list, choose Array I.

Despite the fact that only solvent makes up the fluid within the column initially, adding initial trace concentrations of all dependent species gives a more stable solution to the equilibrium reactions.

### Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the *cA* text field, type CAmax\_inlet\*0.01.
- **4** In the *cB* text field, type CBmax\_inlet\*0.01.
- **5** In the cS text field, type 1e-7.

### SURFACE REACTIONS I (SR)

In the surface reactions interface make sure that the reactions take place on the surface of the beads.

- I In the Model Builder window, under Component 2 (comp2) click Surface Reactions I (sr).
- 2 In the Settings window for Surface Reactions, locate the Boundary Selection section.
- 3 From the Selection list, choose Array I.

#### Reactions I

- I In the Model Builder window, expand the Surface Reactions I (sr) node, then click Reactions I.
- 2 In the Settings window for Reactions, locate the Boundary Selection section.
- 3 From the Selection list, choose Array I.

For the same reason as in the **Transport of Diluted Species** interface, add initial trace concentrations of species A and B.

#### Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the  $cs_A$  text field, type CSOsurf\*0.01.
- **4** In the  $cs_{\rm B}$  text field, type CS0surf\*0.01.

#### LAMINAR FLOW I (SPF)

At the inlet, or the top of the column, atmospheric pressure is applied since the column is open to the surroundings.

Inlet 1

- I In the Model Builder window, under Component 2 (comp2)>Laminar Flow I (spf) click Inlet I.
- 2 In the Settings window for Inlet, locate the Boundary Selection section.
- **3** From the **Selection** list, choose **Inlet**.
- 4 Locate the Boundary Condition section. From the list, choose Pressure.

The average velocity through the *xy*-plane of the geometry is assumed to be constant everywhere along the column height. Set a constant velocity within the column, in this case, at the bottom of the 3D model geometry.

# Outlet I

- I In the Model Builder window, click Outlet I.
- 2 In the Settings window for Outlet, locate the Boundary Selection section.
- **3** From the Selection list, choose Outlet column section.
- 4 Locate the Boundary Condition section. From the list, choose Velocity.
- **5** Locate the **Velocity** section. In the  $U_0$  text field, type U\_column.

#### Symmetry I

- I In the Physics toolbar, click 📄 Boundaries and choose Symmetry.
- 2 In the Settings window for Symmetry, locate the Boundary Selection section.
- 3 From the Selection list, choose Symmetry.

# MULTIPHYSICS

Reacting Flow, Diluted Species 1 (rfd1)

In the Physics toolbar, click An Multiphysics Couplings and choose Domain>Reacting Flow, Diluted Species.

#### MESH I

Select a mesh that resolves the surface of the beads well.

Free Triangular 1

- I In the Mesh toolbar, click  $\bigwedge$  Boundary and choose Free Triangular.
- 2 In the Settings window for Free Triangular, locate the Boundary Selection section.

#### 3 From the Selection list, choose Array I.

#### Size 1

- I Right-click Free Triangular I and choose Size.
- 2 In the Settings window for Size, locate the Element Size section.
- **3** Click the **Custom** button.
- 4 Locate the Element Size Parameters section. Select the Maximum element size check box.
- 5 In the associated text field, type 9E-2.

# Free Tetrahedral I

- I In the Mesh toolbar, click \land Free Tetrahedral.
- 2 In the Settings window for Free Tetrahedral, locate the Domain Selection section.
- 3 From the Geometric entity level list, choose Domain.
- 4 From the Selection list, choose All domains.

#### Size 1

- I Right-click Free Tetrahedral I and choose Size.
- 2 In the Settings window for Size, locate the Element Size section.
- 3 Click the **Custom** button.
- 4 Locate the Element Size Parameters section. Select the Maximum element size check box.
- 5 In the associated text field, type 5E-1.

This model requires that a two-step study node is used. The first step solves the stationary solution of the **Laminar Flow** interface and the second the time-dependent solution for the rest of the interfaces.

# STUDY 2

Stationary

- I In the Study toolbar, click 🔁 Study Steps and choose Stationary>Stationary.
- 2 In the Settings window for Stationary, locate the Physics and Variables Selection section.
- 3 In the table, clear the Solve for check boxes for Reaction Engineering (re),

Chemistry I (chem), Transport of Diluted Species (tds), and Surface Reactions I (sr).

#### Step 1: Time Dependent

- I In the Model Builder window, click Step I: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.
- 3 In the **Output times** text field, type range(0,1,30).

- 4 From the Tolerance list, choose User controlled.
- 5 In the Relative tolerance text field, type 2e-4.
- 6 Locate the Physics and Variables Selection section. In the table, clear the Solve for check box for Laminar Flow I (spf).

Step 2: Stationary

In the Model Builder window, under Study 2 right-click Step 2: Stationary and choose Move Up.

Solution 2 (sol2)

I In the Study toolbar, click The Show Default Solver.

Replace the **Segregated** solver with a **Fully Coupled** one since this fits the quick shifts in concentration originating from the equilibrium reactions in the system. Also apply a **Direct** solver to further improve the stability of the computations.

- 2 In the Model Builder window, expand the Solution 2 (sol2) node, then click Time-Dependent Solver 1.
- **3** In the **Settings** window for **Time-Dependent Solver**, click to expand the **Absolute Tolerance** section.
- 4 From the Tolerance method list, choose Manual.
- 5 In the Absolute tolerance text field, type 1e-4.
- 6 Right-click Time-Dependent Solver I and choose Fully Coupled.
- 7 In the Settings window for Fully Coupled, locate the General section.
- 8 From the Linear solver list, choose Direct.
- 9 In the Model Builder window, click Study 2.
- 10 In the Settings window for Study, locate the Study Settings section.
- II Clear the Generate default plots check box.
- **12** In the **Study** toolbar, click **= Compute**.

# RESULTS

Setup two Sector 3D datasets to rotate the 3D geometry according to its symmetry.

#### Sector 3D 1

- I In the Results toolbar, click **More Datasets** and choose Sector 3D.
- 2 In the Settings window for Sector 3D, locate the Symmetry section.
- **3** In the Number of sectors text field, type 4.
- 4 Click 💽 Plot.

# Sector 3D 2

- I Right-click Sector 3D I and choose Duplicate.
- 2 In the Settings window for Sector 3D, locate the Symmetry section.
- 3 From the Sectors to include list, choose Manual.
- 4 In the Number of sectors to include text field, type 3.
- 5 In the Start sector text field, type 3.
- 6 Click 💽 Plot.

The following step creates Figures 3-6.

# Bulk concentration B

- I In the Results toolbar, click 间 3D Plot Group.
- 2 In the Settings window for 3D Plot Group, type Bulk concentration B in the Label text field.

#### Surface 1

- I Right-click Bulk concentration B and choose Surface.
- 2 In the Settings window for Surface, locate the Data section.
- 3 From the Dataset list, choose Sector 3D I.
- 4 From the Time (s) list, choose 5.
- 5 Click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component 2 (comp2)>Transport of Diluted Species>Species cB>cB Concentration mol/m<sup>3</sup>.
- 6 Click the i Show Grid button in the Graphics toolbar.

#### Bulk concentration B

- I In the Model Builder window, click Bulk concentration B.
- 2 In the Settings window for 3D Plot Group, locate the Data section.
- 3 From the Time (s) list, choose 5.
- 4 In the Bulk concentration B toolbar, click **I** Plot.
- **5** Click the **Com Extents** button in the **Graphics** toolbar.

#### Surface 1

- I In the Model Builder window, click Surface I.
- 2 In the Settings window for Surface, locate the Data section.
- 3 From the Dataset list, choose Sector 3D 2.
- 4 From the Time (s) list, choose 30.

#### Bulk concentration B

- I In the Model Builder window, click Bulk concentration B.
- 2 In the Settings window for 3D Plot Group, locate the Data section.
- 3 From the Time (s) list, choose 30.
- 4 Click the **F** Zoom Extents button in the **Graphics** toolbar.
- 5 In the Bulk concentration B toolbar, click 💽 Plot.

#### Surface concentration B

- I Right-click Bulk concentration B and choose Duplicate.
- 2 In the Settings window for 3D Plot Group, type Surface concentration B in the Label text field.

#### Surface 1

- I In the Model Builder window, expand the Surface concentration B node, then click Surface I.
- 2 In the Settings window for Surface, locate the Data section.
- 3 From the Dataset list, choose Sector 3D I.
- 4 From the Time (s) list, choose 5.
- 5 Click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component 2 (comp2)>Surface Reactions I>Surface species cs\_B>cs\_B Surface concentration mol/m<sup>2</sup>.

#### Surface concentration B

- I In the Model Builder window, click Surface concentration B.
- 2 In the Settings window for 3D Plot Group, locate the Data section.
- 3 From the Time (s) list, choose 5.
- **4** Click the **Transparency** button in the **Graphics** toolbar.
- **5** Click the  $\leftrightarrow$  **Zoom Extents** button in the **Graphics** toolbar.
- 6 In the Surface concentration B toolbar, click 🗿 Plot.

#### Surface 1

- I In the Model Builder window, click Surface I.
- 2 In the Settings window for Surface, locate the Data section.
- 3 From the Dataset list, choose Sector 3D 2.
- 4 From the Time (s) list, choose 30.

#### Surface concentration B

- I In the Model Builder window, click Surface concentration B.
- 2 In the Settings window for 3D Plot Group, locate the Data section.
- **3** From the **Time (s)** list, choose **30**.
- **4** Click the Transparency button in the Graphics toolbar.
- **5** Click the **Com Extents** button in the **Graphics** toolbar.
- 6 In the Surface concentration B toolbar, click 💽 Plot.

#### Velocity field

Last, create Figure 7 to visualize the velocity field within the 3D geometry.

- I In the Home toolbar, click 📠 Add Plot Group and choose 3D Plot Group.
- 2 In the Settings window for 3D Plot Group, type Velocity field in the Label text field.
- 3 Locate the Plot Settings section. Clear the Plot dataset edges check box.

# Streamline 1

- I Right-click Velocity field and choose Streamline.
- 2 In the Settings window for Streamline, locate the Streamline Positioning section.
- **3** From the **Positioning** list, choose **Magnitude controlled**.
- **4** Locate the **Coloring and Style** section. Find the **Line style** subsection. From the **Type** list, choose **Tube**.

#### Color Expression 1

- I Right-click Streamline I and choose Color Expression.
- 2 In the Settings window for Color Expression, locate the Coloring and Style section.
- **3** From the **Color table** list, choose **Twilight**.

#### Surface 1

- I In the Model Builder window, right-click Velocity field and choose Surface.
- 2 In the Settings window for Surface, click to expand the Inherit Style section.
- **3** From the **Plot** list, choose **Streamline I**.

#### Selection I

- I Right-click Surface I and choose Selection.
- 2 In the Settings window for Selection, locate the Selection section.
- **3** From the Selection list, choose All boundaries.
- **4** In the list, select **I**.

- **5** Click  **Remove from Selection**.
- **6** Select Boundaries 2–213 only.
- 7 In the list, select 2.
- 8 Click Remove from Selection.
- 9 Select Boundaries 3–213 only.
- **IO** In the list, select **4**.
- II Click Remove from Selection.
- **12** Select Boundaries 3 and 5–213 only.
- **I3** In the **Velocity field** toolbar, click **I Plot**.
- **I4** Click the **Graphics** toolbar.