Approximation of the Flow Field in Electrochemical Machining Incorporating Pressure Drop Calculation R. Paul¹, M. Hackert-Oschätzchen¹, M. Zinecker¹, A. Schubert¹

Introduction

- Regarded electrochemical machining (ECM) process for machining internal geometries shown in Figure 1
- For process design in ECM material removal simulation models with low computational costs required
- One effective approach: approximate fluid dynamics as two-phase potential flow of electrolyte and gas bubbles
- Due to model assumptions of potential flow, pressure drop not inherently described
- Objective of this work: develop submodel for approximation of pressure drop in ECM



Theory

• Total pressure regarded as a field variable calculated using the PDE

$$-\left(\frac{\vec{u}}{|\vec{u}|}\right) \cdot \nabla p_{\text{tot}} - \nabla \cdot (s_{\text{D}} \nabla p_{\text{tot}}) = f(S, \bar{\varrho}, \bar{u})$$

- At outlet boundary set $p_{tot} = p_{out}$
- Diffusion coefficient s_D to attain numerical stability
- Source term f as function of local working distance S and flow cross-section averages of density ϱ and flow velocity magnitude $u = |\vec{u}|$
- Working distance and flow cross-section averages calculated with additional PDEs using normed auxiliary vector field \vec{v}_{\perp}

Calculation of working distance and cross-section averagesWorking distance SCross-section average \overline{X} of X $S = S_A + S_C$ $\overline{X} := \frac{X_A + X_C}{S}$ $\overline{v}_{\perp} \cdot \nabla S_A - \nabla \cdot (s_D \nabla S_A) = 1$ $\overline{v}_{\perp} \cdot \nabla X_A - \nabla \cdot (s_D \nabla X_A) = X$ $\overline{v}_{\perp} \cdot \nabla S_A - \nabla \cdot (s_D \nabla S_A) = 1$ $\overline{v}_{\perp} \cdot \nabla X_A - \nabla \cdot (s_D \nabla X_A) = X$

Electrolyte flushing

Figure 1. Machining concept of regarded electrochemical machining process



Figure 2. Working distance $S = S_A + S_C$ in arbitrary point *P* as length of the corresponding streamline of \vec{v}_{\perp} for exemplary geometry



$$-v_{\perp} \cdot v_{S_{C}} - v \cdot (s_{D} v_{S_{C}}) = 1 \qquad -v_{\perp} \cdot v_{X_{C}} - v \cdot (s_{D} v_{X_{C}}) = x$$

At anode boundary: $S_A = 0$ At anode boundary: $X_A = 0$ At cathode boundary: $S_C = 0$ At cathode boundary: $X_C = 0$ Remaining boundaries: Zero diffusive flux

• Auxiliary vector field \vec{v}_{\perp} parallel to flow cross-section (Figure 2)

Results

- 2D-axisymmetric simulation of material removal in ECM; electrolyte conductivity based on local temperature and gas volume concentration
- Gas volume concentration influenced by pressure field; pressure field (**Figure 3**) calculated using developed submodel
- Calculation of auxiliary quantities, like cross-section average of flow velocity magnitude shown in Figure 4 compared to local flow velocity

Conclusions

Model is able to describe influence of changes in process parameters and geometry on pressure field and thus on hydrogen volume fraction, effective electrical conductivity and material removal
Computationally efficient tool for ECM process design **Figure 3**. Static pressure p computed using Bernoulli's equation



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Figure 4. Comparison of the flow velocity magnitude u (left) and the crosssectional average velocity \overline{u} (right)



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