

COMSOL Conference 2011, Oct. 26-28, Stuttgart

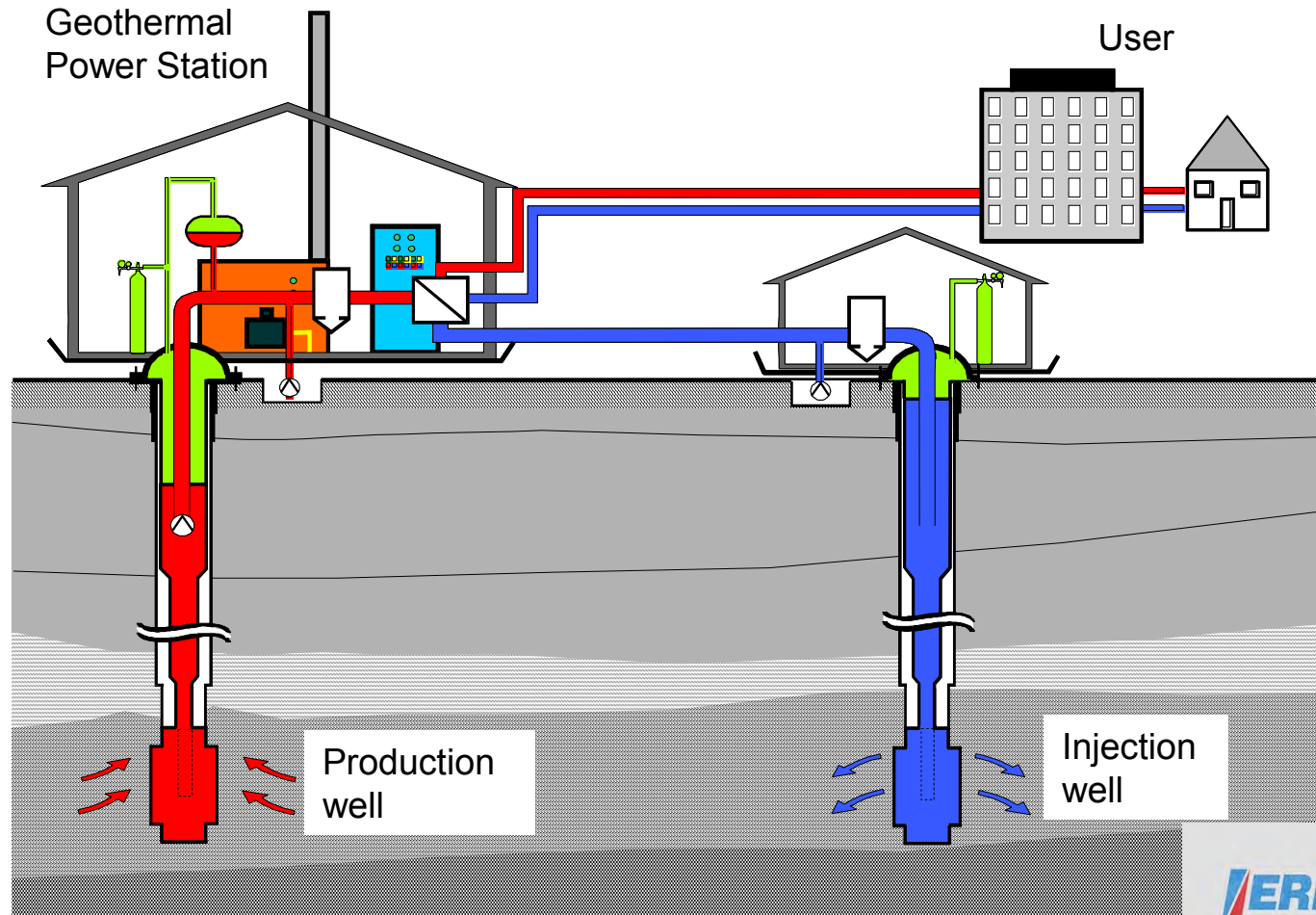
Simulation of Deep Geothermal Heat Production

E. Holzbecher, P. Oberdorfer,
F. Maier, Y. Jin and M. Sauter*

Georg-August-University Göttingen, Geological Sciences,
Goldschmidtstr. 3, Göttingen, Germany

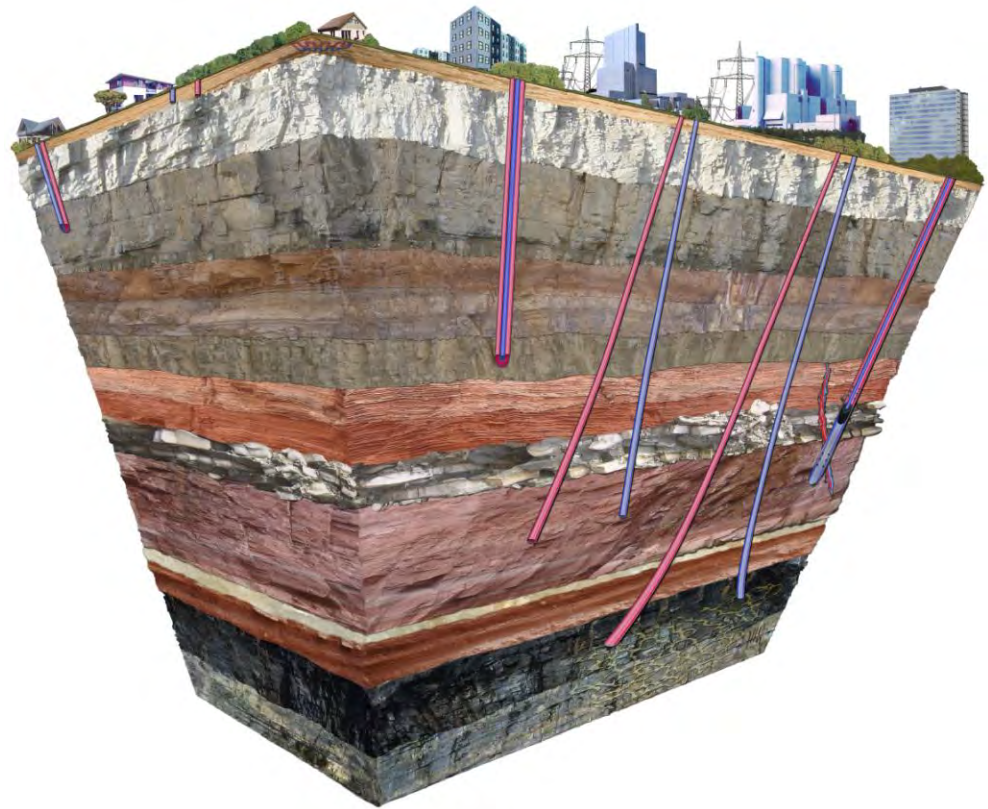


Geothermal Heat Production



gebo

Challenges connected with geothermal heat production from deep reservoirs (5000-7000 m) are currently examined within the collaborative research program "Geothermal Energy and High-Performance Drilling" (gebo), funded by the Ministry of Science and Culture of Lower Saxony (Germany) and Baker Hughes.

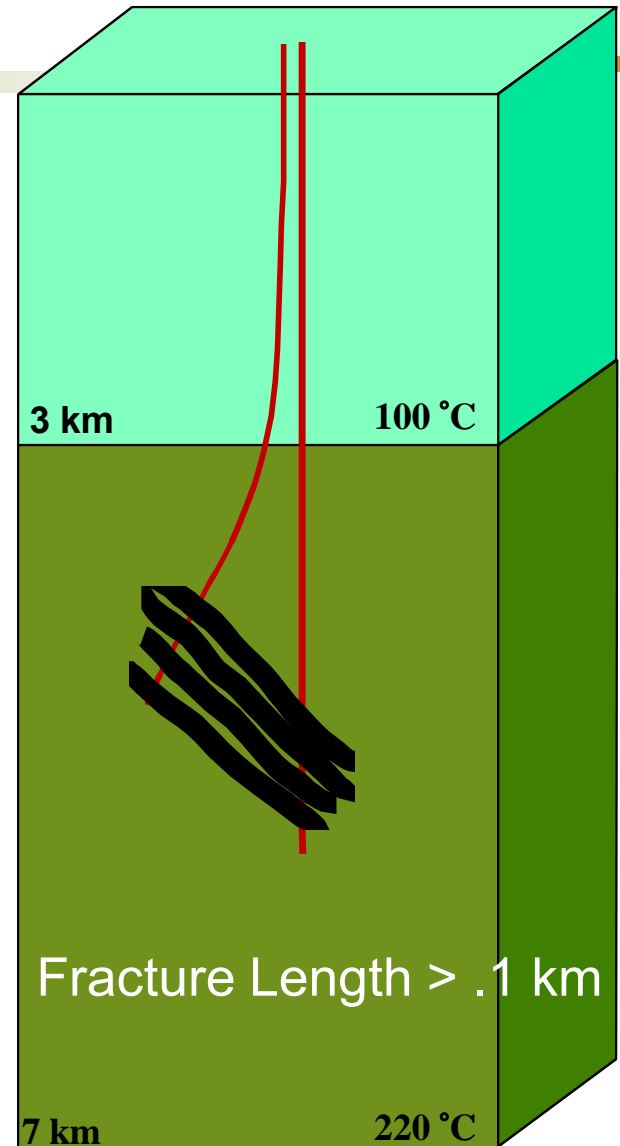


Deep Geothermal Heat Production

Temperature > 100 °C

Depth < 7 km

Flow > 50 m³/h



(from: Jung, Orzol, Schellschmidt)

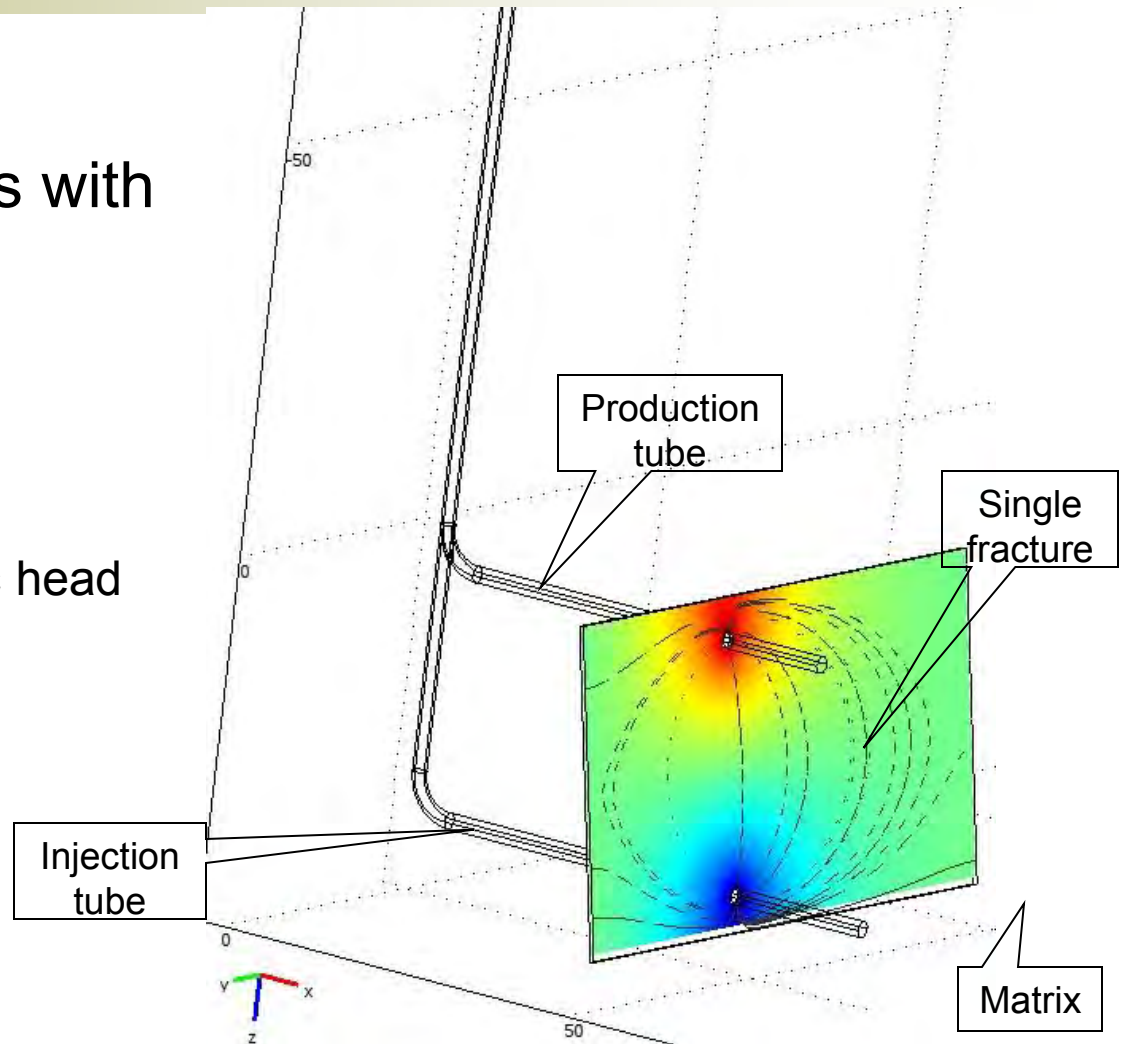
Fracture Model

Fracture connections with

- injection tube
- matrix
- production tube

Fracture flow:

- Surface map for hydraulic head
- Streamlines

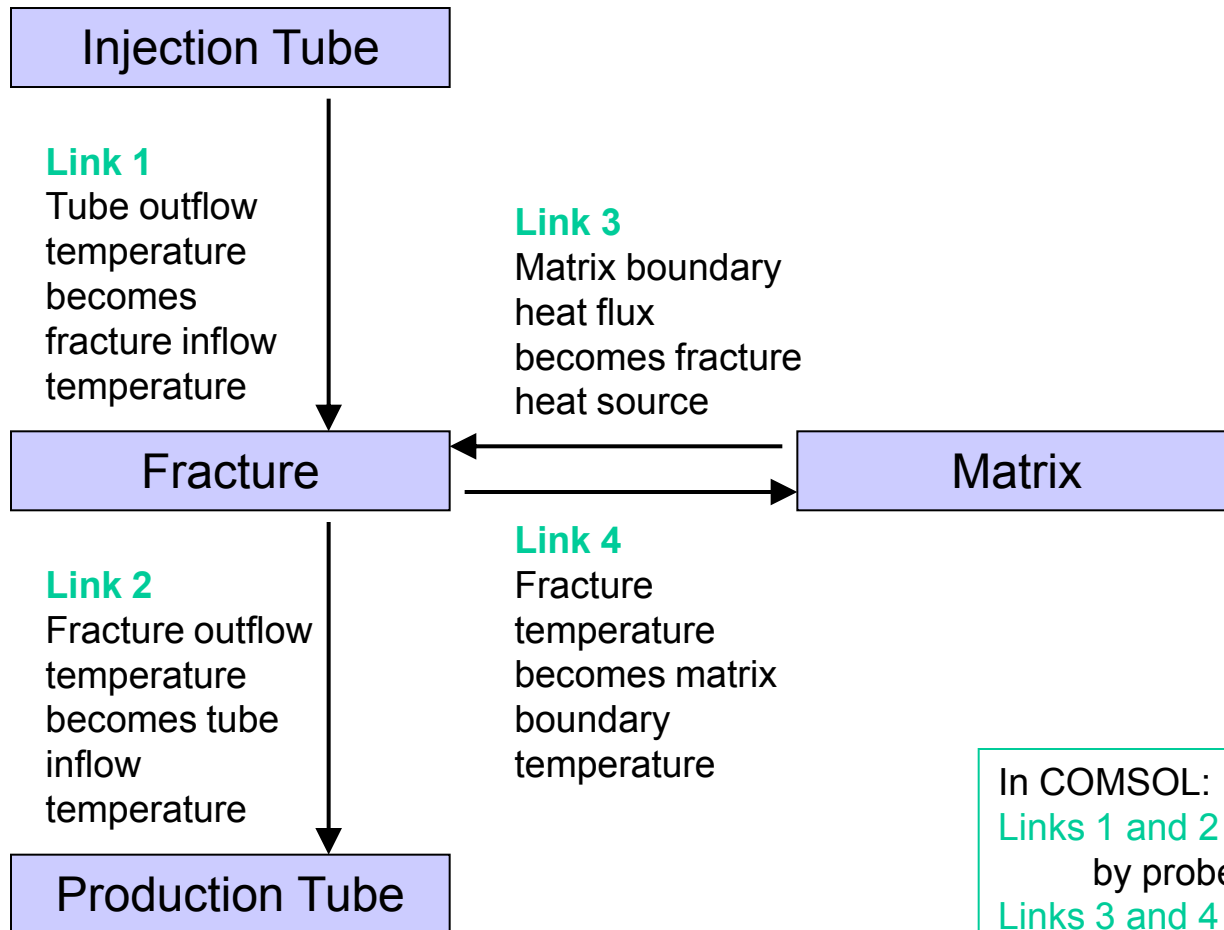


Model Set-up

Model	Dim.	Flow	Cond./ Conv.	Transvers. heat flux neglected	Convect. heat flux neglected
Injection tube	1	Free Fluid	both	x	
Fracture	2	Darcy / Free Fluid	both	x	
Matrix	3	no Flow	cond. only	*	x
Production tube	1	Free Fluid	both	x	

* In most conventional models, transversal heat in the matrix is neglected, (following Vinsome & Westerveld).

Couplings / Links



In COMSOL:
Links 1 and 2
by probes, unidirectional
Links 3 and 4
by extrusions

Further Dependencies & Couplings

Temperature dependency of

- fluid thermal conductivity
- fluid heat capacity

within heat
flow mode

- fluid density
- viscosity

between
flow and
transport

Not yet considered !

Pde - Flow Options

■ Matrix

- No-flow **X**
- Darcy's Law

■ Fracture

- Darcy's Law
- Potential flow **X**
- Navier-Stokes equations
- Brinkman equations
- [Hagen-Poiseuille Law (for slices)]

■ Tubes

- 1D constant **X**
- [Hagen-Poiseuille Law (for tubes)]
- [Navier-Stokes equations]

Example: Brinkman equation
(steady state)

$$\frac{\eta}{\mathbf{k}} \mathbf{u} + \nabla p - \frac{\eta}{\theta} \nabla \left(\nabla \mathbf{u} + (\nabla \mathbf{u})^T \right) = 0$$

$$\nabla \cdot \mathbf{u} = 0$$

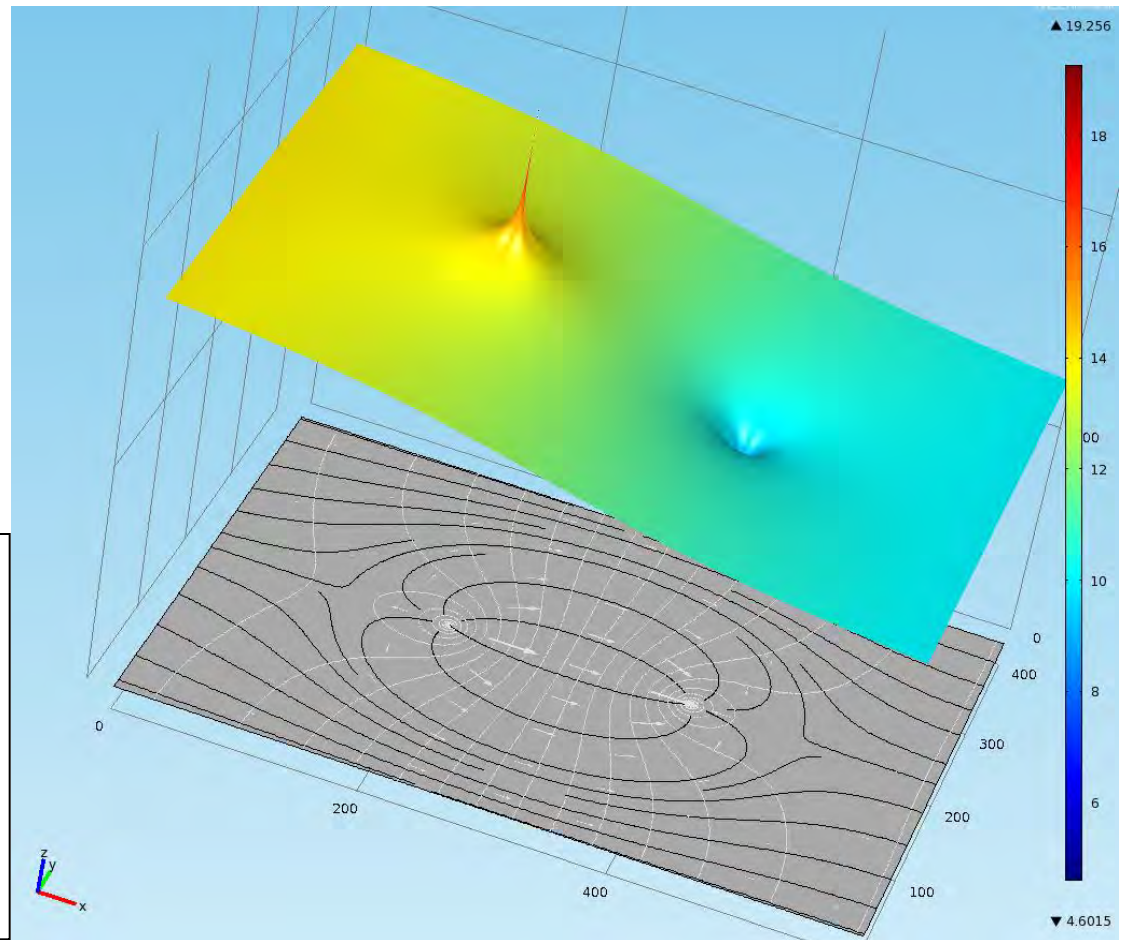
with symbols

\mathbf{u} Darcy velocity
 \mathbf{k} permeability tensor
 η dynamic viscosity
 p pressure
 θ porosity

Doublet: Analytical Solution

For potential flow

- potential surface
- streamlines (black)
- potential contours (white)
- velocity vector field



Pde – Heat Flow Options

- Matrix
 - Heat Transfer in Solids
 - Heat Transfer in Porous Media
 - pde - mode **X**
- Fracture
 - Heat Transfer in Fluids **X**
 - Heat Transfer in Porous Media
 - pde - mode
- Tubes
 - Heat Transfer in Fluids **X**
 - pde - mode

Example:

Heat transfer in porous media

$$(\rho C)^* \frac{\partial T}{\partial t} = \nabla k \nabla T - (\rho C)_f \mathbf{u} + Q = 0$$

with symbols

\mathbf{u}	Darcy velocity
k	thermal conductivity
$(\rho C)^*$	heat capacity of solid/fluid
$(\rho C)_f$	fluid heat capacity
Q	heat source / sink

Meshing

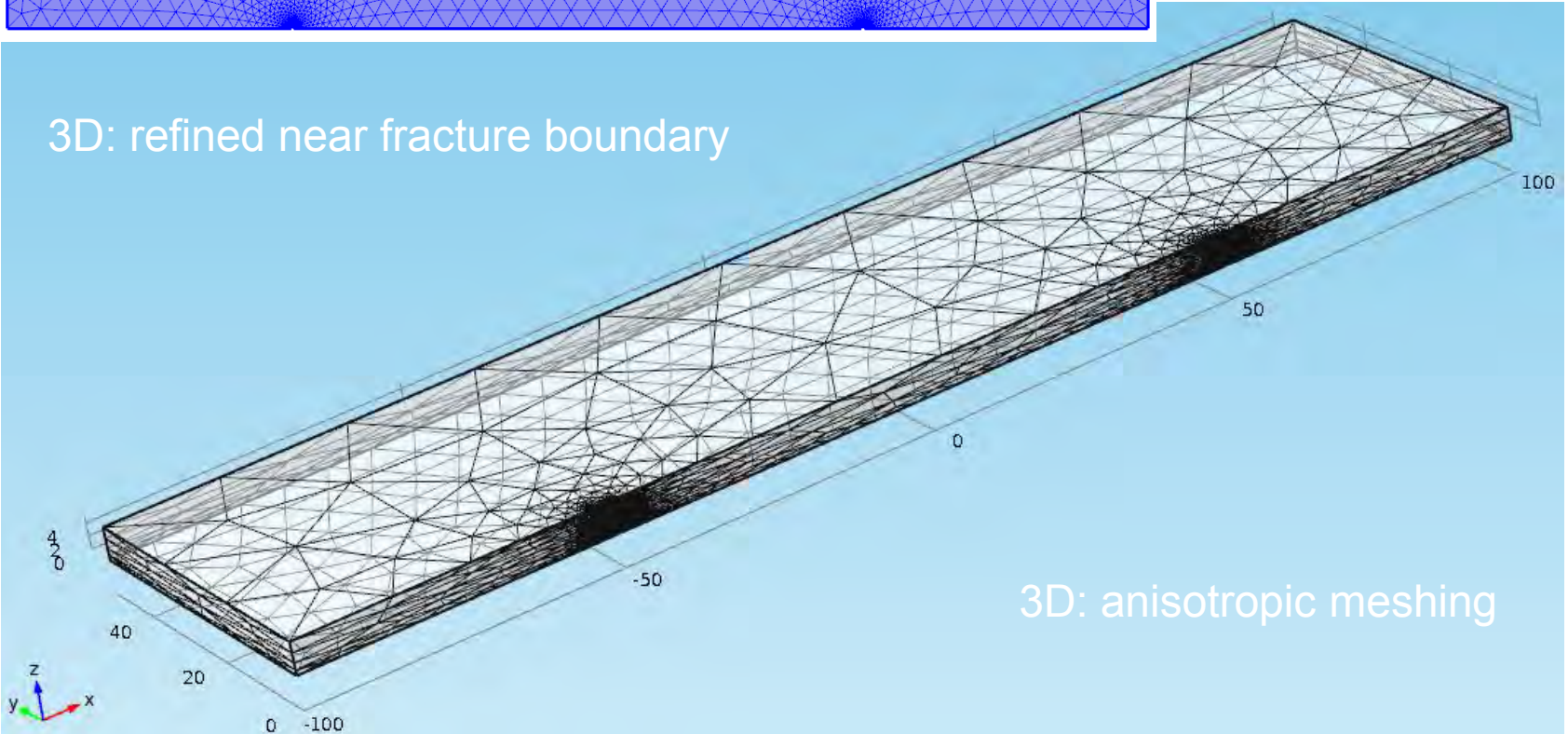
2D: refined near inlet and outlet

3467 elements

19170 elements

3D: refined near fracture boundary

3D: anisotropic meshing

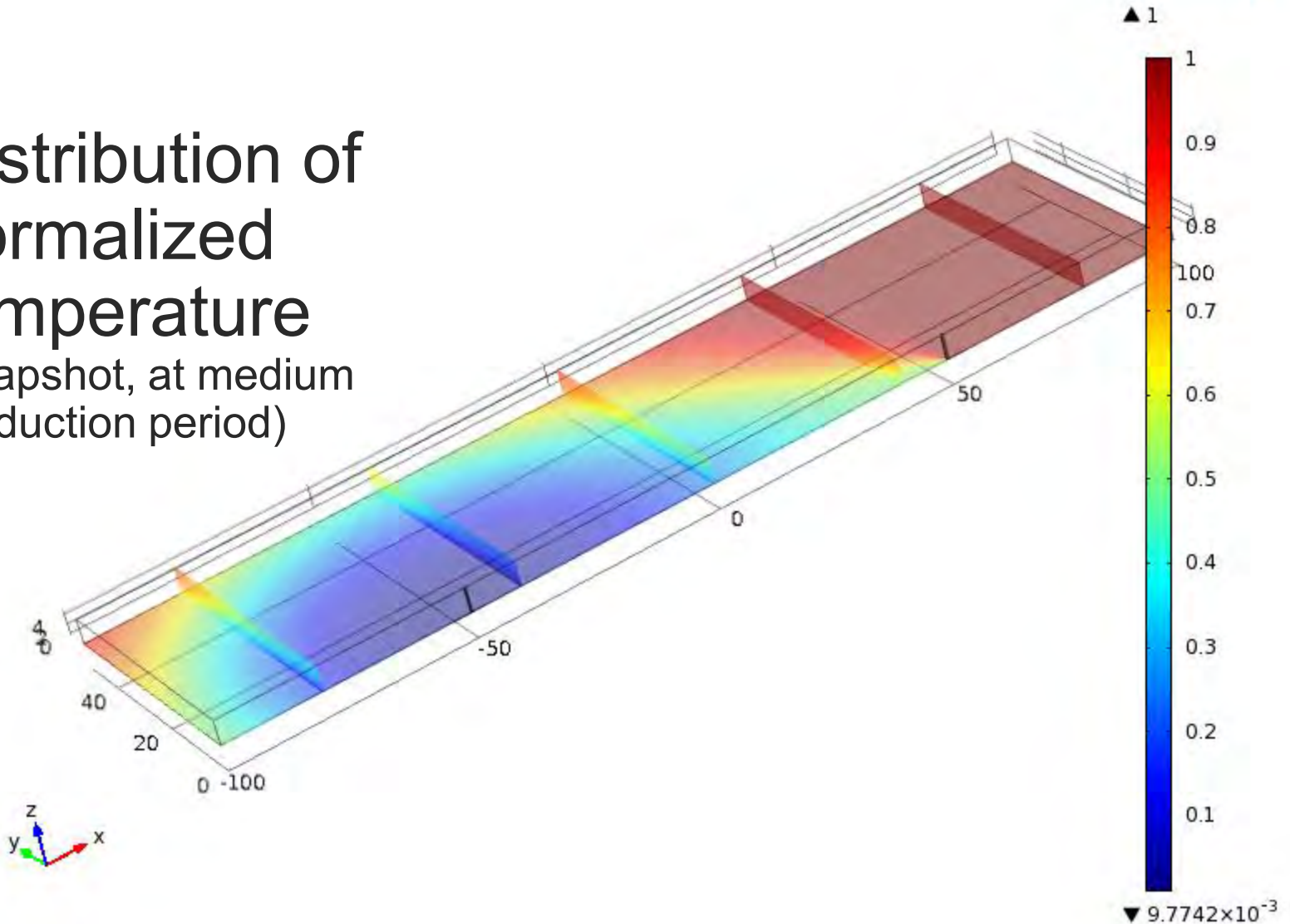


Input Data

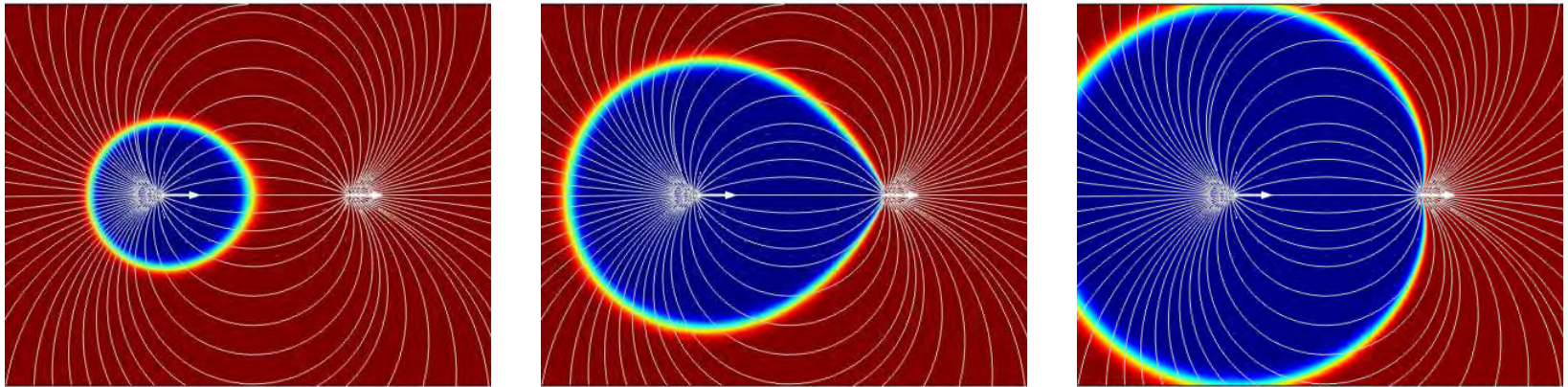
<i>Name</i>	<i>Value</i>	<i>Unit</i>	<i>Name</i>	<i>Value</i>	<i>Unit</i>
Inlet temperature	70	°C	Fracture porosity	0.6	-
Reservoir temperature	200	°C	Fracture hydraulic conductivity	$1.5 \cdot 10^{-2}$	m/s
Reservoir depth	5000	m	Fracture heat capacity	1000	J/kg/°C
Geothermal gradient	0.038	°C/m	Fracture thickness	0.002	M
Doublet distance	100	m	Longitudinal dispersivity	1	m
Borehole diameters	9 5/8, 7	inch	Transversal dispersivity	0.1	m
Total pumping/ Injection rate	0.115	m ³ /s	Matrix thickness	5	m
Velocities in boreholes	0.62, 1.16	m/s	Matrix thermal conductivity	2	W/m/°C
Fracture length	250	m	Time period	$1.5 \cdot 10^6$	s
Fracture density	2000	kg/m ³			

Results: Matrix Heat Transfer

Distribution of normalized temperature (snapshot, at medium production period)

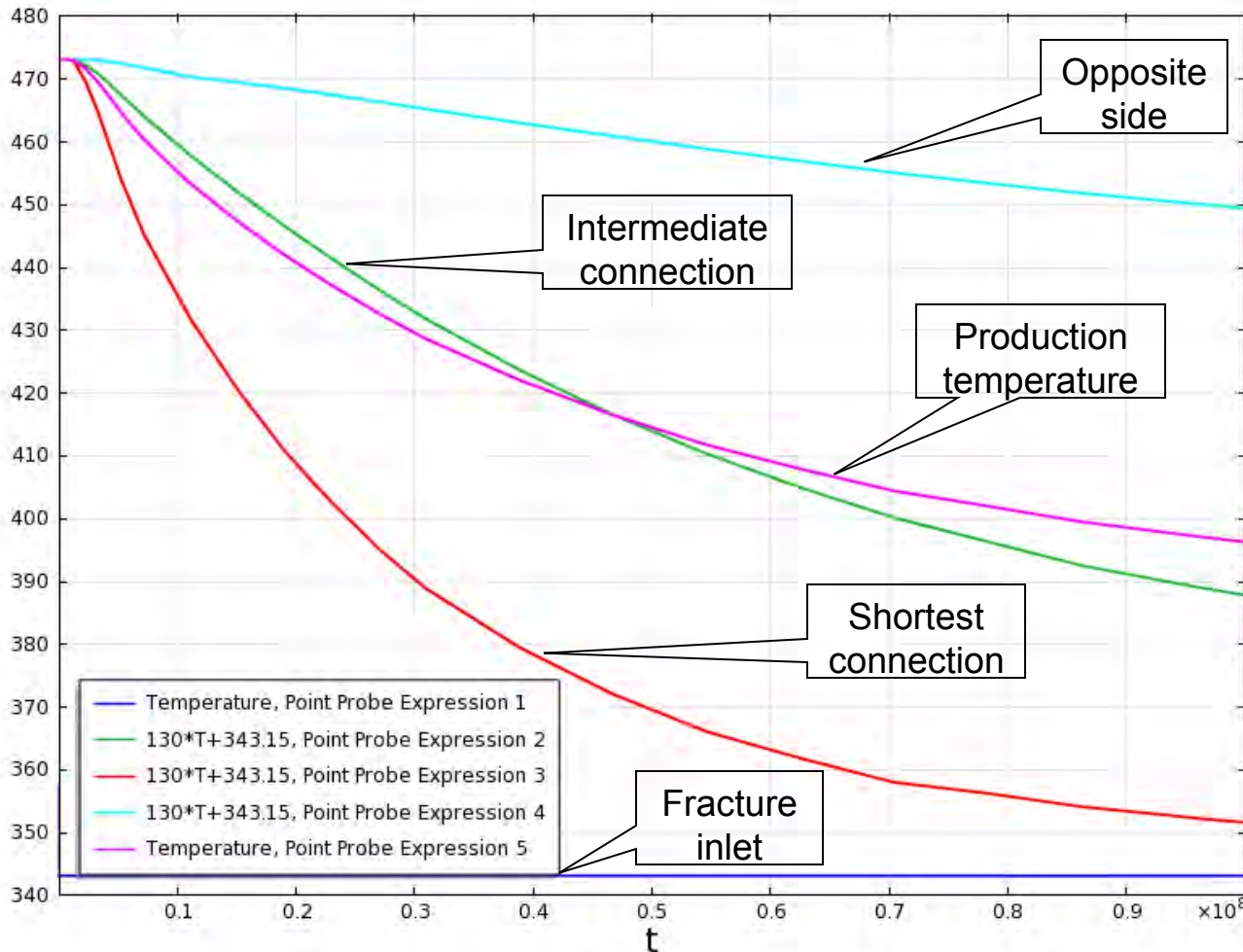


Results: Fracture Heat Flux



Cold water plume at three different stages of geothermal production

Results: Breakthrough Curves



Temperatures [°K] at sub-model couplings and final production, in dependence of time [s]

Conclusions

- The model approach is superior to the conventional method, in which transversal heat transfer in the matrix is neglected

-
- Using COMSOL Multiphysics, models of different dimensionality can be coupled easily
 - Couplings can be uni-directional or two-directional
 - Couplings can be realized by
 - extrusions, if the same geometry is shared by both models
 - Probes, if only single valued functions have to be transferred

[Lookout]

We intend a comparison

- concerning the different pde-approaches in COMSOL
- with results from a similar study using the cellular automata approach (performed at Techn. Univ. Braunschweig)

Acknowledgement:

The authors appreciate the support of 'Niedersächsisches Ministerium für Wissenschaft und Kultur' and 'Baker Hughes' within the GeBo G7 project.